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Direct kinetic evidence for the electronic effect of ruthenium in PtRu on the dissociative adsorption of methanol

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A R T I C L E I N F O

ABSTRACT

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1. Introduction

Direct methanol fuel cells (DMFC) are appealing as a power source due to the high energy density and easy handling of the liquid methanol fuel [1,2]. Among the various bimetallic combinations that have been studied, PtRu has been accepted as the best electrocatalyst for the methanol oxidation reaction (MOR) in DMFC [3–5]. The two global reactions that comprise the overall MOR are (i) the initial dehydrogenation step culminating in various intermediates like CO that poison the Pt sites,

$$CH_3OH + Pt \rightarrow Pt - CO + 4H^+ + 4e^-$$
(1)

and (ii) the slow oxidation of the poisoning intermediates to retrieve the active sites,

$$Pt - CO + H_2O \rightarrow Pt + CO_2 + 2H^+ + 2e^-.$$
(2)

In this regard, a bifunctional theory was advanced to account for the promotional effect of the secondary metal. Briefly, the bifunctional model considers Pt sites as adsorption/dehydrogenation centers while Ru acts as the center generating oxygen containing species at lower potentials for the oxidation of the intermediates (Reaction 2) formed at the Pt sites (Reaction 1) [6,7]. Another relevant model considers the electronic effect of Ru on Pt. Accordingly, electron donation by Ru to Pt

Dissociative adsorption of methanol on platinum in a PtRu bimetallic electrocatalyst has been studied by an accelerated degradation test and normal pulse voltammetry. PtRu electrodes with a minimum number of potential cycles show the highest electrode rate constant values while the one with platinum-like surface characteristics show the lowest rate constant values, evidencing the promotional effect of Ru.

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decreases the Pt-4f binding energy, which in turn reduces the Pt—CO bond strength, enabling a facile removal of the CO intermediate [7]. The electronic effect of Ru has also been suggested to render Pt more susceptible for dissociative adsorption of methanol [8].

The limitations to a systematic analysis of the effect of Ru on the initial dissociative adsorption of methanol are (i) the kinetics of methanol oxidation is complicated involving multi-step electrode reactions and parallel pathways forming poisonous intermediates, (ii) the activity of Pt towards the dissociative adsorption of methanol cannot be compared quantitatively, for example, between Pt and PtRu since the electrochemical active surface area of Pt in PtRu cannot be estimated precisely, and (iii) standard potential (E^0) of dissociative adsorption of methanol on Pt and PtRu is unknown and hence the corresponding standard rate constants cannot be estimated from the voltammetric experiments for evaluating electrocatalysts kinetically. We present here a methodology to circumvent the above limitations as much as possible and observe the electronic effect of Ru on the dissociative adsorption of methanol on Pt in a PtRu electrocatalyst in terms of rate constants. The strategies involved in our study are (i) the two global reactions reactions 1 and 2 can be decoupled with the aid of normal pulse voltammetry (NPV) with short electrolysis time so that the reaction is stopped at the formation of soluble intermediates without progressing to the extent of poisoning the electrocatalyst [9,10], (ii) accelerated degradation cycles (ADC) can be employed to gradually leach out Ru in PtRu to an extent wherein the surface of the PtRu electrocatalyst is devoid of Ru and/or its effect [11,12], and (iii) even without the knowledge of E^0 , the rate constants for different electrocatalysts can be compared at convenient reference potentials as suggested by Oldham and Parry [13].

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2. Experimental

NPV studies were carefully designed so as to renew the depletion layer of the reactants for each new pulse without contaminating with the products of the previous pulse. This was achieved by waiting at a base potential for a period of 25 s. Furthermore, a very thin layer of catalyst was applied onto glassy carbon substrate (3 mm diameter) by drop casting 2 µL of the ink prepared typically by sonicating 2 mg of 20 wt.% commercial PtRu on carbon support (1:1 atomic ratio; E-TEK) in 2 mL of water and ethanol mixture (1:1) containing 15 µL of 5% Nafion. A series of ADC-NPV experiments were conducted as follows. The carbon supported PtRu electrode (PtRu/C) was scanned at 0.02-1.2 V for 5, 20, 40, 60, 80, and 100 cycles in 0.5 M H₂SO₄ at a rate of 50 mV s⁻¹, where the initial five cycles can be considered as cleaning cycles. After each specified number of cycles, the electrolyte was replaced with 0.5 M H₂SO₄ and 1 M methanol and the NPV experiments were conducted subsequently. A series of NPV experiments were performed after a specified number of ADCs on the electrodes, which are denoted as PtRu/C-5cy, PtRu/C-20cy, PtRu/C-40cy, PtRu/C-60cy, PtRu/C-80cy, and PtRu/C-100cy. The base potential was deduced from a cyclic voltammogram that was recorded before each NPV experiment [10]. A Hg/HgSO₄ electrode served as the reference electrode, and the potentials are referred subsequently with respect to RHE. A Pt wire was used as a counter electrode. The solutions were purged with high purity nitrogen for 10 min before the experiments and blanketed gently over the solution during the experiments. CO stripping voltammetry was carried out by purging high purity CO gas for 30 min at a holding potential of 0.1 V. The purging gas was then switched to nitrogen to remove dissolved CO. CO_{ad} was then stripped by scanning potential between 0.05 and 1.2 V at a rate of 20 mV/s. The amounts of Ru ions in H₂SO₄ solution were measured using inductively coupled plasma-optical emission spectroscopy (ICP-OES, Perkin-Elmer).

3. Results and discussion

Xu et al. [10] showed that by applying potential pulses of shorttime (<30 ms) and waiting for large periods between successive pulses, the total electrooxidation of methanol on a polycrystalline Pt can be confined to the formation of soluble species like formic acid and/or formaldehyde:

$$CH_3OH + H_2O \rightarrow HCOOH + 4H^+ + 4e^-$$
 (3)

The above reaction has a rate determining step of initial dissociative adsorption of methanol, viz.

$$CH_3OH_{sol} \rightarrow CH_2OH_{ad} + H^+ + e^-$$
 (4)

Making use of reaction 3, the electronic effect of Ru on the dissociative adsorption of methanol on Pt was studied by NPV. A gradual dissolution of Ru from PtRu/C surface was realized by potential cycling between 0.02 and 1.2 V in 0.5 M H₂SO₄. Fig. 1a shows the changes in the voltammograms of PtRu/C to that of Pt through 100 cycles. The changes include fully developed hydrogen adsorption/desorption peaks, decrease in the double layer current, and shifting of Pt oxide reduction peak to anodic potentials. Fig. 1b shows CO stripping voltammograms measured after various potential cycles. Initially the peak potential is 0.57 V, typical of PtRu, which after 100 cycles increases to 0.77 V indicating Pt like surface. A shoulder at higher potential appears after 60 cycles and becomes dominant after 100 cycles. Fig. 1c shows concentrations of dissolved Ru and Pt after various potential cycles measured by ICP-OES. NPV studies were conducted on the electrodes obtained after a specified number of ADCs. Typical S-shaped voltammograms at different sampling times (τ) are shown in Fig. 2. The anodic limiting currents (i_d) vary inversely with τ , and the half wave potentials $(E_{1/2})$ shift anodically with decreasing τ . Fig. 3 shows the variation of anodic limiting current with



Fig. 1. (a) Cyclic voltammograms of 100 cycles of PtRu/C in 0.5 M $H_2SO_{4_1}$ (b) CO stripping voltammograms of PtRu/C at various potential cycles, and (c) variation of dissolved Ru and Pt concentrations with potential cycles.

the inverse square root of τ for various PtRu/C electrodes. The linear variation indicates, as per Cottrell equation (Eq. (5)), that i_d is diffusion-controlled and semi-infinite [14].

$$i_{\rm d}(\tau) = \frac{nFAC\sqrt{D_{\rm app}}}{\sqrt{\pi\tau}} \tag{5}$$

where D_{app} denotes apparent diffusion coefficient of methanol and other symbols have the usual electrochemical significance [14]. The D_{app} values obtained from the slope of the plots in Fig. 3 vary closely in the order of 10^{-11} cm² s⁻¹ and are in agreement with the



Fig. 2. Normal pulse voltammograms typical of methanol oxidation on PtRu/C-5cy in 0.5 M H₂SO₄ and 1 M methanol at 25 °C: (a) $\tau = 16$, (b) $\tau = 20$, (c) $\tau = 22$, (d) $\tau = 24$, and (e) $\tau = 26$ ms.

literature values [10]. Based on Butler-Volmer model [14], the current (i)-potential (E) behavior of the rate determining step (reaction 4) in the case of irreversible electrode process can be given as

$$E = E_{1/2} - \frac{0.0542}{\alpha n_{\alpha}} \log\left(\frac{i_{\rm d} - i}{i}\right) \tag{6}$$

where α is the anodic transfer coefficient. Fig. 4a shows a linear $\left(\frac{i_{\rm d}-i}{i_{\rm d}-i}\right)$ variation of the logarithmic term with *E* for a τ value of 24 ms at various PtRu/C electrodes. The transfer coefficient values estimated from the slope of the plots vary between 0.30 ± 0.05 and 0.35 ± 0.05 . The $E_{1/2}$ values estimated using Eq. (6) are 0.729, 0.735, 0.745, 0.770, 0.777, and 0.790 V, respectively, with an accuracy of \pm 5 mV, for the electrodes PtRu/C-5cy, PtRu/C-20cy, PtRu/C-40cy, PtRu/C-60cy, PtRu/C-80cy, and PtRu/C-100cy, indicating a clear trend of relatively facile rate determining step at PtRu/C-5cy to a more sluggish kinetics at PtRu/C-100cy - the electrode with Pt-like surface characteristics.

The relation between $E_{1/2}$ and the standard rate constant k_0 in the case of irreversible electrode process is given by the equation [13],

$$E_{1/2} = E^0 - \frac{2.303RT}{\alpha n_{\alpha} F} \log\left(\frac{4k_0 \sqrt{\tau}}{\sqrt{3D_{\text{app}}}}\right)$$
(7)



Fig. 3. Variation of i_d with $\tau^{-0.5}$ at various PtRu/C electrodes in 0.5 M H₂SO₄ and 1 M methanol at 25 °C.



Fig. 4. (a) Variation of $\log\left(\frac{i_d-i}{i}\right)$ and (b) apparent methanol oxidation rate constant with *E* at various PtRu/C electrodes at 25 °C. $\tau = 24$ ms.

Since E^0 could not be obtained voltammetrically, the corresponding k_0 could not be obtained using Eq. (7). Under the circumstances wherein the E^0 is unknown, Oldham and Parry [13] proposed to determine the rate constant at some convenient reference potential E_r for the purpose of comparing, as in our case, related electrode systems. The elegance of this method is illustrated in Fig. 4b. Instead of a single $E_{\rm r}$ value, a range of values between 0.15 and 0.45 V was considered since there is a good possibility of E^0 falling in this potential range [10], and the corresponding rate constant values were computed using Eq. (7) and the values for $E_{1/2}$, α , τ , and D_{app} . Since the Butler–Volmer kinetics is implicit, the rate constants for each electrode system increase exponentially with E_r (Fig. 4b). The variation of the rate constant with *E* is highest in the case of PtRu/C-5cy followed by, in the order, PtRu/C-20cy>PtRu/C-40cy>PtRu/C-60cy>PtRu/C-80cy>PtRu/ C-100cy. During Ru dissolution, the best configuration for methanol adsorption, viz. an ensemble of 3 Pt atoms with at least one adjacent Ru atom (10 at.% of Ru) [15], might be lost between 40 and 60 potential cycles. Therefore, a relatively large drop between the curves pertaining to PtRu/C-40cy and PtRu/C-60cy is observed in Fig. 4b. The plots of Fig. 4b provide direct electrochemical evidence in terms of rate constants for the electronic model that predicts the modification of Pt electronic structure by Ru, making it more susceptible for dissociative adsorption of methanol.

4. Summary

A direct kinetic evidence for the promotional effect of Ru in PtRu on the initial dissociative adsorption of methanol on Pt is provided, favoring the electronic effect model. Furthermore, the methodology used here can be applied to evaluate the effect of a second metal on the initial methanol adsorption and compare its effect on CO oxidation with various compositions. Therefore, by balancing between these two important reaction sequences in MOR, it is possible to design an optimal composition of a binary electrocatalyst.

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